

Non-iridium-based electrocatalyst for durable acidic oxygen evolution reaction in proton exchange membrane water electrolysis

Received: 8 January 2022

Accepted: 7 September 2022

Published online: 20 October 2022

 Check for updates

Zhen-Yu Wu^{1,9}, Feng-Yang Chen^{1,9}, Boyang Li^{2,9}, Shen-Wei Yu³, Y. Zou Finrock⁴, Debora Motta Meira⁵, Qiang-Qiang Yan⁶, Peng Zhu¹, Ming-Xi Chen⁶, Tian-Wei Song⁶, Zhouyang Yin³, Hai-Wei Liang⁶, Sen Zhang³✉, Guofeng Wang²✉ and Haotian Wang^{1,7,8}✉

Iridium-based electrocatalysts remain the only practical anode catalysts for proton exchange membrane (PEM) water electrolysis, due to their excellent stability under acidic oxygen evolution reaction (OER), but are greatly limited by their high cost and low reserves. Here, we report a nickel-stabilized, ruthenium dioxide (Ni-RuO₂) catalyst, a promising alternative to iridium, with high activity and durability in acidic OER for PEM water electrolysis. While pristine RuO₂ showed poor acidic OER stability and degraded within a short period of continuous operation, the incorporation of Ni greatly stabilized the RuO₂ lattice and extended its durability by more than one order of magnitude. When applied to the anode of a PEM water electrolyser, our Ni-RuO₂ catalyst demonstrated >1,000 h stability under a water-splitting current of 200 mA cm⁻², suggesting potential for practical applications. Density functional theory studies, coupled with operando differential electrochemical mass spectroscopy analysis, confirmed the adsorbate-evolving mechanism on Ni-RuO₂, as well as the critical role of Ni dopants in stabilization of surface Ru and subsurface oxygen for improved OER durability.

Water electrolysis using renewable electricity is widely recognized as a promising and sustainable route to the production of clean hydrogen (H₂) fuels^{1–3}. Currently the dominant alkaline water electrolysis (AWE) technology suffers from challenges including the crossover of product gases, high ohmic resistance, limited current density and low operating pressure, mainly because of utilization of a diaphragm and a

liquid electrolyte in the AWE device^{4,5}. Using a polymer-based proton exchange membrane (PEM) for efficient proton transfers, PEM water electrolysis (PEM-WE) technology can effectively tackle the above challenges with markedly enhanced performance, and is thus attracting broad research interest^{4–7}. However, the large-scale deployment of PEM-WE devices is largely obstructed by the lack of active, stable and

¹Department of Chemical and Biomolecular Engineering, Rice University, Houston, TX, USA. ²Department of Mechanical Engineering and Materials Science, University of Pittsburgh, Pittsburgh, PA, USA. ³Department of Chemistry, University of Virginia, Charlottesville, VA, USA. ⁴Structural Biology Center, X-ray Science Division, Argonne National Laboratory, Lemont, IL, USA. ⁵Canadian Light Source Inc., Saskatoon, Saskatchewan, Canada. ⁶Department of Chemistry, University of Science and Technology of China, Hefei, China. ⁷Department of Materials Science and NanoEngineering, Rice University, Houston, TX, USA. ⁸Department of Chemistry, Rice University, Houston, TX, USA. ⁹These authors contributed equally: Zhen-Yu Wu, Feng-Yang Chen, Boyang Li. ✉e-mail: sz3t@virginia.edu; guw8@pitt.edu; htwang@rice.edu

low-cost acidic oxygen evolution reaction (OER) catalysts^{5,8–15}. Most existing OER catalysts with excellent performance in alkaline solutions, however, are hampered by sluggish reaction kinetics in acids^{5,8,11,16}. More importantly, they suffer from severe degradation under strong acidic and oxidative conditions^{5,6,9,17}. It is highly desired, but remains a major challenge, to develop active and durable acidic OER electrocatalysts.

Currently iridium (Ir)-based catalysts such as IrO₂ are generally considered the only practical OER electrocatalysts in PEM devices due to their robust durability and good activity^{9,10,14,17–20}. However, their high cost and extremely low earth abundance greatly limit their large-scale application^{5,9}. Although ruthenium (Ru) has been recognized as an attractive alternative to Ir for acidic OER (~7.5 times cheaper than Ir)^{12,21–24}, and while its oxides (for example, RuO₂) typically present good acidic OER activity, Ru-based catalysts are still greatly challenged by their OER long-term stability in acids or PEM reactors^{12,13,24–26}. In recent years great efforts have been made to improve Ru acidic OER performance via strategies such as multimetal oxides or doping (Sr_{0.90}Na_{0.10}RuO₃ (ref. 22), Cr_{0.6}Ru_{0.4}O₂ (ref. 23), Mn-doped RuO₂ (ref. 27), Ni/Co-doped RuO₂ (refs. 28,29)), morphology and structure tuning (ultra-thin RuO₂ nanosheets³⁰, single-atom Ru-N-C²⁶), strain effect (Ru₁-Pt₃Cu¹²), reconstruction (A₂Ru₂O₇, A=Y, Nd, Gd and Bi³¹) and so on, resulting in enhanced OER activity and stability compared with commercial RuO₂ nanoparticles in acids. Nevertheless, the stability of most Ru-based catalysts reported to date remains limited to within tens of hours under a low current density of ~10 mA cm⁻², which is far from industrial application requirements^{12,23,27,32}. More importantly, the stability performance obtained under the standard three-electrode set-up with acidic liquid electrolyte may not necessarily be translated into a practical PEM reactor due to significant variation in their reaction environments⁹.

Generally, the acidic OER stability challenge of Ru-based catalysts is mainly a result of the following two reasons. The first is related to the oxidative release of lattice oxygen, which can cause overoxidation of Ru species into dissolvable RuO₄ under OER potentials^{9,12,33–35}. The second is the direct demetallation of surface Ru, which can also result in crystal structure collapse of Ru-based catalysts^{35–37}. Therefore, simultaneous stabilization of lattice oxygen and surface Ru in RuO₂ catalysts under OER conditions could be a feasible way to boost its stability in acids. Here we report an exciting result that, by incorporation of nickel (Ni) dopants in RuO₂ nanocrystals, we were able to markedly improve stabilization of the RuO₂ lattice for extended durability under acidic OER conditions. The impact of Ni incorporation on RuO₂ stability is impressive: while pristine RuO₂ showed poor OER stability (<40 h of operation under a 10-mA cm⁻² OER current on a rotation disc electrode (RDE)), our Ni-doped RuO₂ (Ni-RuO₂) catalyst showed a stable operation of >200 h with no obvious degradation. More impressively, once coupled to a commercial Pt/C hydrogen evolution reaction (HER) catalyst in a practical PEM electrolyser, our Ni-RuO₂ catalyst showed stable water electrolysis of >1,000 h at 200 mA cm⁻², suggesting its great potential for practical water-splitting applications. Density functional theory (DFT) studies and operando differential electrochemical mass spectroscopy (DEMS) analysis confirmed the adsorbate-evolving mechanism (AEM) for RuO₂ catalysts and clearly showed that Ni dopants can enhance the lattice stability of surface Ru and subsurface oxygen, which is responsible for its improved OER durability. Additionally, our Ni-RuO₂ catalyst also exhibited much improved activity, which needs a small overpotential of 214 mV to deliver 10-mA cm⁻² OER current and a cell voltage of 2.10 V (without ohmic loss compensation or iR compensation) to deliver 1.5-A cm⁻² overall water-splitting current under room temperature.

Synthesis and characterization of catalysts

We developed a three-step process to incorporate Ni into the RuO₂ lattice for Ni-RuO₂ catalyst preparation (Methods and Fig. 1a). First, a wet impregnation of metal precursors was adopted on a carbon black

support, which was followed by H₂/Ar annealing reduction to obtain Ru₃Ni nanoparticles supported on carbon black (Ru₃Ni/C; Fig. 1b and Supplementary Figs. 1a and 2). The carbon support is important during this process in regard to the prevention of particle aggregation³⁸. Second, the obtained Ru₃Ni/C was annealed in air to convert Ru₃Ni nanoparticles to Ru₃NiO_x and, meanwhile, to remove the carbon supports (Supplementary Figs. 1b and 3). Finally, the obtained Ru₃NiO_x underwent an acid-leaching process to remove unstable Ni species and yield the final catalyst—that is, Ni-RuO₂. The air-annealing and acid-leaching processes greatly enhanced acidic OER performance (Supplementary Fig. 4a), and the optimized air-annealing temperature was found to be 450 °C (Supplementary Fig. 4b). The choice of Ni incorporation over other transition metals (Supplementary Fig. 5), and the Ru:Ni precursor molar ratio of 3:1 (Supplementary Figs. 6–11), were determined after a rigorous performance optimization process.

The X-ray diffraction (XRD) pattern of Ni-RuO₂ showed the characteristic peaks of rutile RuO₂ (JCPDS 71-2273) with the dominant (110) peak at 28.1° (Supplementary Fig. 1c), suggesting that incorporation of Ni did not affect the RuO₂ lattice structure. Transmission electron microscopy (TEM) and high-angle annular dark-field scanning TEM (HAADF-STEM) images (Fig. 1c–e and Supplementary Fig. 12) clearly showed that Ni-RuO₂ nanoparticles were uniform in size, with an average diameter of ~4.0 nm (Fig. 1c, inset). This ultrafine nanoparticle size inherited from its precursor (that is, Ru₃Ni/C), in which Ru₃Ni nanoparticles had an average size of only 1.7 nm (Fig. 1b). High-magnification HAADF-STEM images clearly revealed that Ni-RuO₂ nanoparticles exhibited high crystallinity, with distinct lattices observed (Fig. 1d and Supplementary Fig. 12b–d). By focusing on individual nanoparticles, we observed well-defined lattice fringes that can be ascribed to the {110} planes of RuO₂ (Fig. 1e,f). Another TEM image also showed a series of RuO₂ lattices, including (110) and (210) (Supplementary Fig. 13). Successful incorporation of Ni was confirmed by energy-dispersive spectroscopic (EDS) elemental mapping (Fig. 1g and Supplementary Figs. 14 and 15). Ni distribution was uniform across the entire RuO₂ matrix. We also synthesized RuO₂ nanoparticles without incorporation of Ni (that is, RuO₂) as a control sample. The RuO₂ catalyst showed morphology similar to that of Ni-RuO₂, with an average nanoparticle size of ~4.5 nm (Supplementary Fig. 16), as well as high crystallinity, as confirmed by XRD (Supplementary Fig. 17a).

Electronic properties of catalysts

The X-ray photoelectron spectroscopy (XPS) survey spectrum (Supplementary Fig. 18a) revealed an Ni atomic ratio of 1.4 at.% (Ni:Ru ratio, ~1:21) in Ni-RuO₂. There were four peaks in the high-resolution Ni 2p XPS spectrum (Fig. 2a): peaks at 856.0 and 873.9 eV were assigned to Ni 2p_{3/2} and Ni 2p_{1/2} of Ni²⁺, respectively, and those at 861.8 and 881.6 eV were ascribed to two accompanying satellites^{39,40}. For high-resolution Ru 3d XPS spectra, two sets of doublet peaks were observed between 280 and 290 eV (Fig. 2b), which could be attributed to the doublet peaks of Ru⁴⁺ 3d_{5/2}, 3d_{3/2} and their satellite peaks^{23,24}. The binding energy of Ru 3d_{5/2} and 3d_{3/2} for Ni-RuO₂ was positively shifted (-0.1 eV) compared with that of RuO₂, possibly suggesting that Ru in the Ni-RuO₂ catalyst presented a slightly higher oxidation state than that in RuO₂ (see the X-ray absorption near-edge spectroscopy (XANES) spectra below for additional evidence). Previous studies revealed that Ru species with a higher oxidation state could enhance their OER activity^{30,41}. In high-resolution O 1s XPS spectra (Supplementary Fig. 18b), peaks at 530.1, 531.3 and 532.9 eV were found to be Ru-O bonds, OH groups and H₂O, respectively^{42,43}. Compared with RuO₂, the Ru-O bonds and OH groups in Ni-RuO₂ were slightly negatively shifted.

We then performed X-ray absorption spectroscopy (XAS) on both Ni-RuO₂ and RuO₂ (Fig. 2c–i). The Ni K-edge XANES suggested that the Ni oxidation state in Ni-RuO₂ was very close to NiO of +2 (Fig. 2c). The corresponding extended X-ray absorption fine-structure (EXAFS) spectrum of Ni-RuO₂ at the Ni K-edge showed a dominant peak at

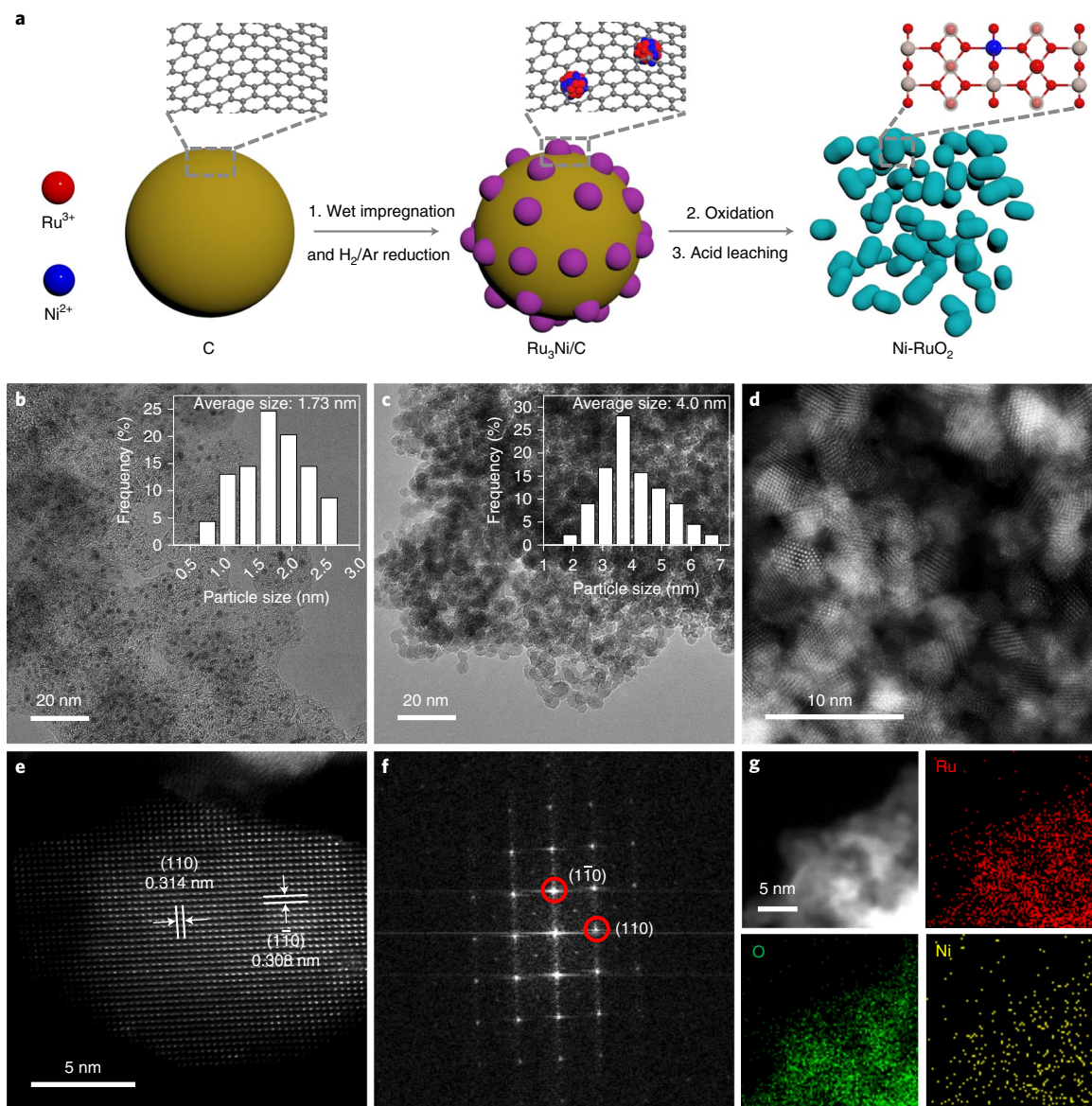


Fig. 1 | Synthesis and characterization of Ni-RuO₂. **a**, Schematic illustrating the synthesis of Ni-RuO₂. **b, c**, TEM images of Ru₃Ni/C (**b**) and Ni-RuO₂ (**c**), showing the very small size of Ru₃Ni and its derived Ni-RuO₂ nanoparticles. **d, e**, HADDF-STEM images under different magnifications of Ni-RuO₂. **d** is a low-magnification HADDF-STEM image, and **e** is a high resolution HADDF-STEM image.

f, Corresponding fast Fourier transform pattern of **e**. **g**, EDS mapping of the Ni-RuO₂ catalyst. Nanoparticle sizes are ~1.73 nm for Ru₃Ni and ~4 nm for Ni-RuO₂, as shown in the insets of **b, c**, respectively. The distinct lattice in **e** suggests the high crystallinity of our Ni-RuO₂ catalyst.

around 1.6 Å (Fig. 2d), which was assigned to the Ni-O coordination. No obvious NiO or Ni metal nanoparticles were formed in Ni-RuO₂ as suggested by the distinct EXAFS spectrum compared with the NiO or Ni reference, respectively, which indicates a high dispersion of Ni in the RuO₂ lattice. This Ni-O coordination environment in Ni-RuO₂ was further confirmed by wavelet transform (WT) of its Ni K-edge, where one strong peak intensity was observed (Fig. 2g–i). We also analysed the XANES and EXAFS spectra of Ni-RuO₂ and RuO₂ at the Ru K-edge. While these two Ru K-edges appeared to be very close (Fig. 2e), a zoomed-in XANES spectrum revealed Ni-RuO₂ showing a slightly higher near-edge absorption energy and white line peak than those in RuO₂ (Supplementary Fig. 19), suggesting a relatively higher Ru oxidation state in Ni-RuO₂, which agrees well with the XPS analysis. The Ru K-edge EXAFS spectrum of Ni-RuO₂ is almost identical to that of RuO₂, suggesting the same coordination structures before and after the incorporation of Ni (Fig. 2f and Supplementary Fig. 20). The above characterizations clearly suggested that Ni dopants were uniformly distributed in the

RuO₂ lattice, in which Ru oxidation states were slightly shifted due to the incorporation of Ni atoms.

Electrochemical characterization on a RDE in acidic electrolyte

Following OER standard measurements^{12,13,23,24}, we first evaluated OER activities of the Ni-RuO₂ catalyst and control samples on a RDE set-up. The control samples were as-prepared RuO₂ and commercial RuO₂ nanoparticles (Com-RuO₂; see Supplementary Figs. 17b and 21 for characterizations). Linear sweep voltammetry (LSV) curves showed that our as-synthesized RuO₂ presented better OER activity than Com-RuO₂, mainly due to particle size effects (Fig. 3a and Supplementary Fig. 22). The overpotential for Com-RuO₂ to deliver 10 mA cm⁻² was 330 mV, consistent with previous reports^{12,30}. Incorporation of Ni showed an obvious enhancement in the OER activity of RuO₂; the overpotential for Ni-RuO₂ to reach 10 mA cm⁻² was 214 mV, lower than that of RuO₂ (227 mV). This overpotential difference was quickly increased

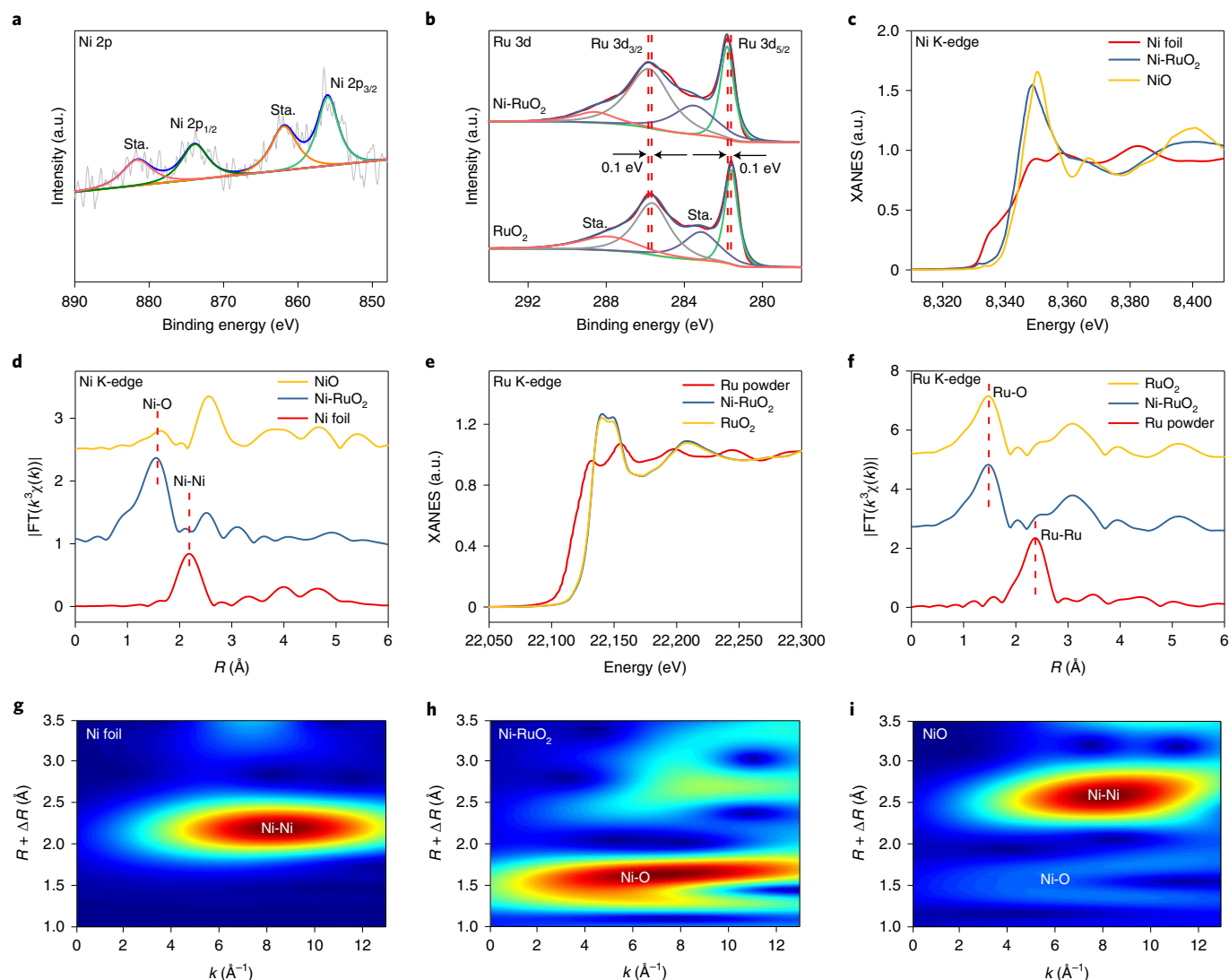


Fig. 2 | Electronic structure of Ni-RuO₂ and RuO₂. **a, b**, High-resolution XPS spectra of Ni 2p (**a**) and Ru 3d (**b**). **c, d**, XANES (**c**) and EXAFS (**d**) spectra at the Ni K-edge of Ni-RuO₂, indicating incorporation of Ni into RuO₂ nanocrystals. **e, f**, XANES (**e**) and EXAFS (**f**) spectra at the Ru K-edge, suggesting a well-defined RuO₂

structure for Ni-RuO₂ after incorporation of Ni. **g–i**, WT of the Ni K-edge for Ni foil (**g**), Ni-RuO₂ (**h**) and NiO (**i**), demonstrating highly dispersed Ni dopants in the Ni-RuO₂ catalyst. a.u., arbitrary units; Sta., satellite peak; R, bond length; FT, Fourier transform; k, wave vector.

following delivery of higher current densities, due to the significantly improved Tafel slope of Ni-RuO₂ (42.6 mV dec⁻¹) compared with both RuO₂ (52.9 mV dec⁻¹) and Com-RuO₂ (60.7 mV dec⁻¹) (Fig. 3b). Electrochemical impedance spectroscopy (EIS) of Ni-RuO₂ at 1.45 V showed the lowest charge transfer resistance (Fig. 3c), suggesting enhanced OER kinetics compared with RuO₂ and Com-RuO₂^{24,30}. The superior activity of Ni-RuO₂ can be reliably repeated (Supplementary Fig. 22a), and is among the best compared with other reported acidic OER catalysts (Supplementary Table 1).

To better understand the origin of the high OER performance of Ni-RuO₂, we first tested electrochemical double-layer capacitance (C_{dl}) to calculate the electrochemically active surface area (ECSA) and roughness factor (R_f) for activity normalization (Fig. 3d, Supplementary Fig. 23a–c and Supplementary Table 2). Our prepared Ni-RuO₂ and RuO₂ with ultrafine nanocrystal structures clearly showed higher C_{dl} and ECSA than those of Com-RuO₂ (Fig. 3d and Supplementary Table 2). In particular, Ni-RuO₂ had the highest C_{dl} and ECSA, nearly twice those in RuO₂, suggesting that incorporation of Ni can significantly improve the density of active sites. Considering ECSA-normalized OER activity, specific activity still followed the order Ni-RuO₂ > RuO₂ > Com-RuO₂

(Fig. 3e), suggesting intrinsically improved OER activity on the Ni-RuO₂ catalyst due to incorporation of Ni.

While achieving high OER activity is important, good stability may play an even more important role in practical water-splitting applications^{9,17}. We investigated OER durability in acidic electrolyte at 10 mA cm⁻² on RDE (Fig. 3f), a widely adapted benchmark criterion in literature^{10,12,24}. Although our synthesized RuO₂ showed improved stability compared with Com-RuO₂, its performance still degraded at a rapid rate and lasted no longer than 40 h. This performance degradation was markedly mitigated by incorporation of Ni. Our Ni-RuO₂ presented a negligible potential increase after 200 h of continuous operation, suggesting a much more stabilized structure compared with RuO₂ under acidic OER conditions. This was also confirmed by cyclic voltammogram (CV) tests (Supplementary Fig. 24). The excellent durability of Ni-RuO₂ outperformed state-of-the-art, non-Ir-based acidic OER catalysts reported in RDE tests (Fig. 3g and Supplementary Table 1). We used inductively coupled plasma mass spectrometry (ICP-MS) to examine the electrolyte during chronopotentiometry stability testing of Ni-RuO₂ (Supplementary Fig. 25a). This yielded only ~10 ppb of Ru and 1 ppb of Ni in the electrolyte after stability testing,

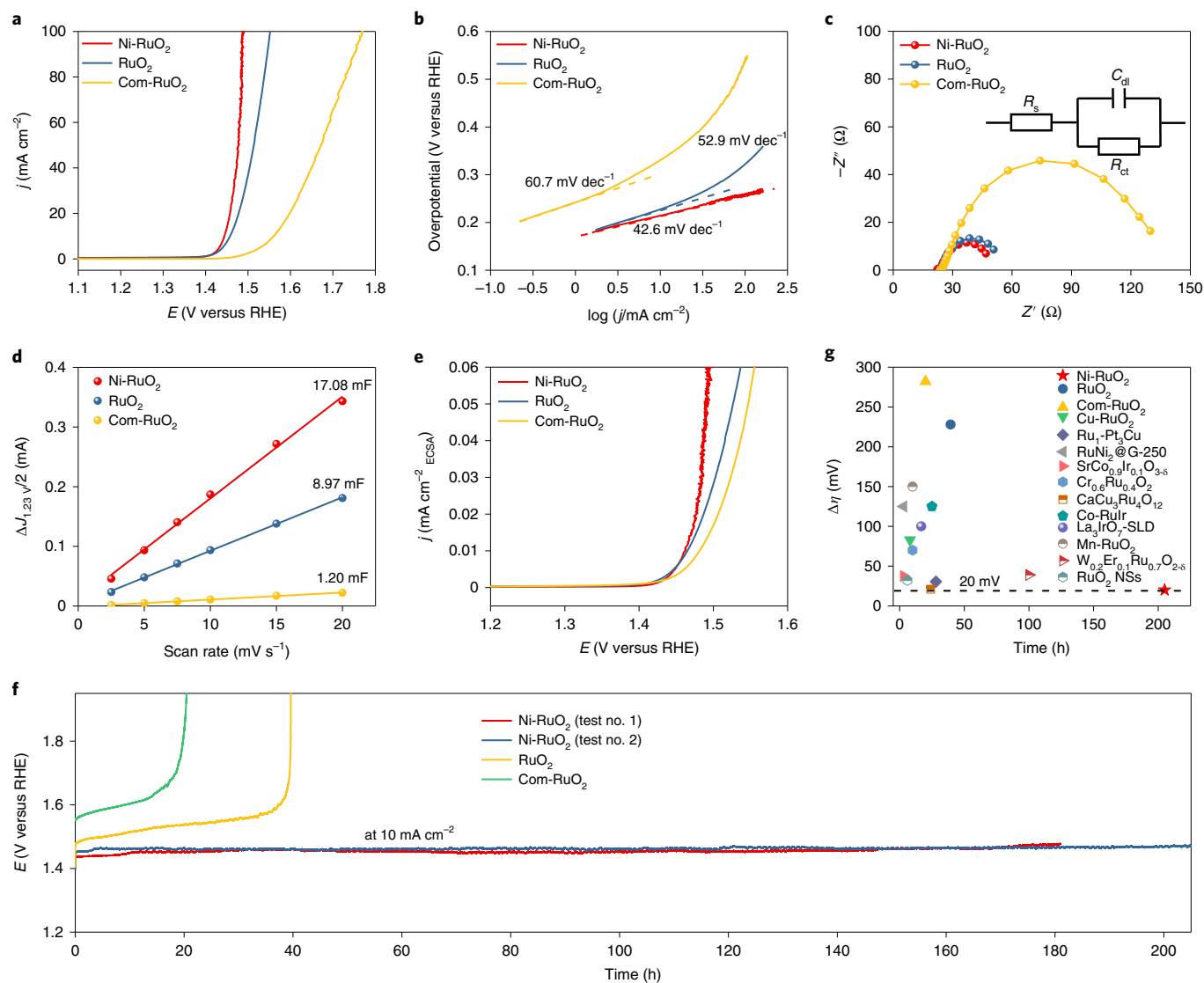


Fig. 3 | Acidic OER performance on RDE. **a,b**, LSV curves (**a**) and Tafel slopes (**b**) of Ni-RuO₂, RuO₂ and Com-RuO₂. **c**, EIS plots of Ni-RuO₂, RuO₂ and Com-RuO₂. X-axis (Z'), real part; Y-axis ($-Z''$), imaginary part. **d**, C_{dl} plots derived from CV curves. **e**, ECSA-normalized LSVs of Ni-RuO₂, RuO₂ and Com-RuO₂.

f, Stability tests of Ni-RuO₂, RuO₂ and Com-RuO₂. **g**, Comparison of the stability of our catalysts in acidic electrolyte with that of reported catalysts. j , current density; J , current.

representing ~3.3% of the total material. The stability number (S) was 7.4×10^5 at 205 h for Ni-RuO₂ (Supplementary Fig. 25b), which is comparable with rutile IrO₂ (-10^6 ; Alfa-Aesar)¹⁷ and other reported IrO₂ (-10^5 ; Sigma-Aldrich)⁴⁴, further demonstrating the excellent stability of Ni-RuO₂. No obvious changes were observed in either Ni and Ru K-edge of Ni-RuO₂ under in situ XAS measurements (Supplementary Figs. 26–28). Furthermore, we systematically characterized post-catalysis Ni-RuO₂, which suggested that both structures and properties of the catalyst were retained well (Supplementary Figs. 29–33). The excellent OER durability of Ni-RuO₂ compared with pristine RuO₂ clearly indicates the critical role of Ni incorporation.

Understanding the mechanism

We performed DFT simulations to understand the effects of Ni dopants on OER performance, in particular the stability of the RuO₂ catalyst. Consistent with our XRD observation (Supplementary Fig. 1c), RuO₂ crystals were modelled to have a rutile lattice structure. Moreover, we chose to study the catalytic properties of the fully oxidized (110) surface of RuO₂ (Fig. 4a and Supplementary Fig. 34a) because that was

predicted to be the most stable surface in our RuO₂ catalyst annealed at 450 °C^{21,45,46}. In the outermost layer of the RuO₂ (110) surface there are two types of Ru site: the coordinatively unsaturated site (CUS) and the fully coordinated bridge site (BRI). The Ru atom has five coordinated O atoms at a CUS Ru site but binds to six O atoms at a BRI site⁴⁷. Our DFT results indicate that it would be energetically favourable for a Ni dopant to replace the BRI Ru site rather than the CUS site (Supplementary Fig. 35). Additionally, simulated EXAFS based on this proposed atomic structure agrees well with our experimental tests (Supplementary Fig. 36). We thus adopted such a Ni-doped RuO₂ (110) surface to examine the impacts of incorporation of Ni on the OER process (Fig. 4b and Supplementary Fig. 34b).

As depicted schematically in Fig. 4c, a 4e⁻ OER on RuO₂ (110) is derived from H₂O adsorption at a CUS Ru site, followed by two sequential deprotonation steps to form *OH and then *O. Subsequently, the reaction pathway bifurcates into one of two possible mechanisms: lattice oxygen mechanism (LOM) or AEM^{12,15,24,36}. Following LOM, surface-adsorbed *O further reacts with a lattice O to produce O₂ whereas the generated O vacancy is refilled by another H₂O. Following

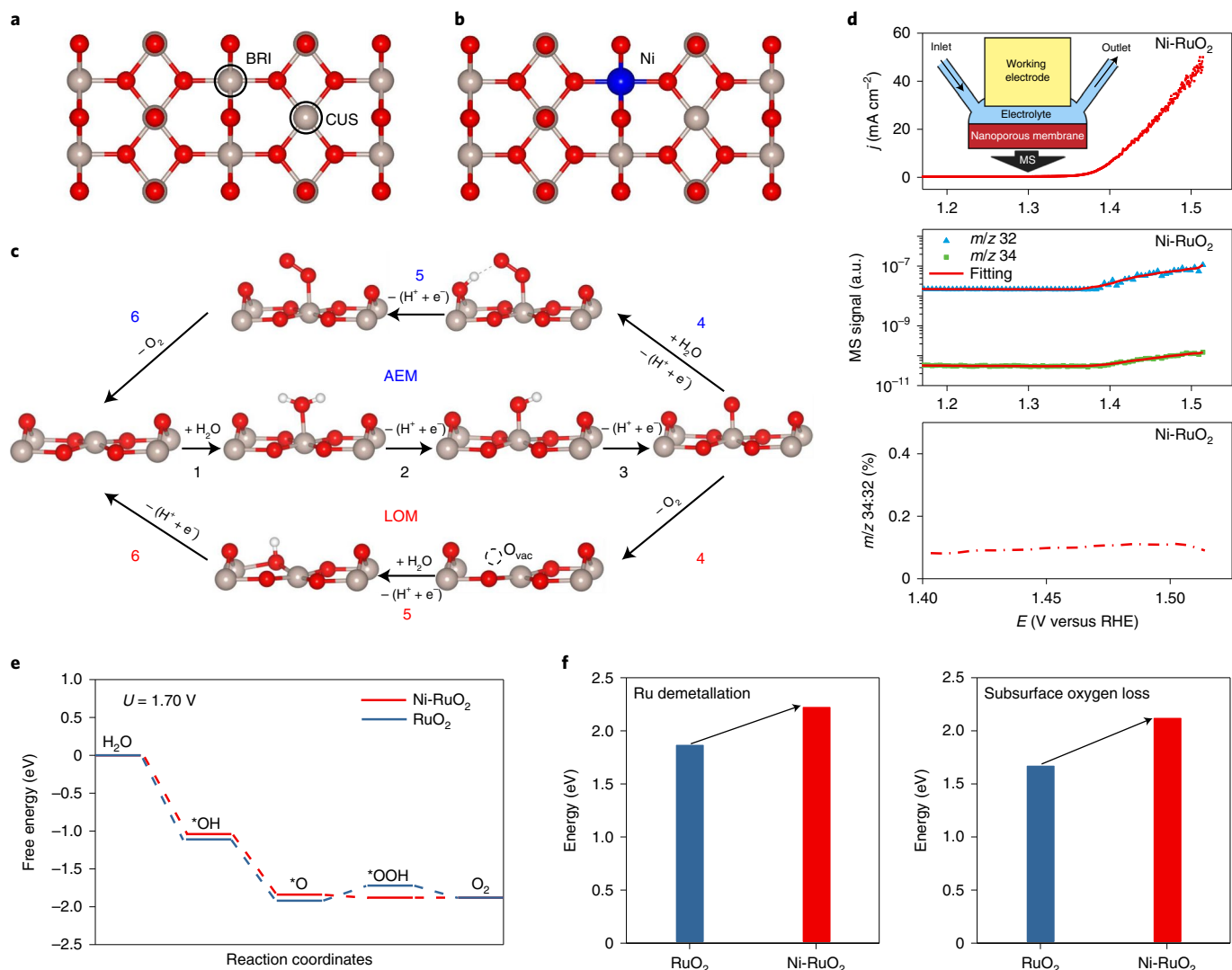


Fig. 4 | Understanding the mechanism. **a, b**, Atomistic structures of the surfaces of RuO₂ (110) (**a**) and Ni-RuO₂ (110) (**b**). **c**, Schematic illustration of AEM and LOM for OER on the RuO₂ (110) surface. Grey, blue, red and white balls represent Ru, Ni, O and H atoms, respectively. **d**, DEMS measurements. Top: CV cycle without iR compensation; middle: DEMS signals of ³²O₂ (¹⁶O + ¹⁶O) and ³⁴O₂ (¹⁶O + ¹⁸O) collected during the CV cycle; bottom: ratio of ³⁴O₂:³²O₂, which

remained unchanged with increase in potential, suggesting that ³⁴O₂ was derived from background ¹⁸O rather than from the lattice. Inset: schematic illustration of the DEMS device used. **e**, Computed free energy evolution of OER via AEM on surfaces of RuO₂ (110) and Ni-RuO₂ (110) under an electrode potential of 1.70 V. **f**, Calculated energies for structural degradation of surfaces of RuO₂ (110) and Ni-RuO₂ (110).

AEM, the surface-adsorbed O further reacts with another H₂O in the electrolyte to form *OOH and then the final product of O₂. We note that hydrogen bonds between H and an adjacent O helped stabilize OOH adsorption at the CUS Ru site on the RuO₂ (110) surface (Supplementary Fig. 37)^{47,48}. Supplementary Fig. 38 shows the DFT-predicted free energy evolution for OER via AEM on the RuO₂ (110) surface. The OER limiting potential, defined as the lowest potential under which free energy evolution becomes downhill, is about 1.89 V on the RuO₂ (110) surface. Additionally, the rate-determining step for OER on the RuO₂ (110) surface was predicted to be the step of O transformation to OOH (Supplementary Note 1), consistent with a previous result^{24,27}. In contrast, the limiting potential for OER via LOM was predicted to be 3.76 V (Supplementary Fig. 39), which is 1.87 V higher than that of AEM. This result suggests the OER on the RuO₂ (110) surface would be thermodynamically more favourable to follow the AEM mechanism rather than the LOM, consistent with a previous study³⁶.

To experimentally confirm this AEM pathway, we conducted operando DEMS measurements via the isotope ¹⁸O-labelling method

(Fig. 4d and Supplementary Fig. 40). First we 'labelled' RuO₂ and Ni-RuO₂ catalysts with ¹⁸O by performing OER under constant current density (Methods). If lattice oxygen is exchanged, the catalyst surface would be labelled by ¹⁸O. We then measured the isotope signal of evolved O₂ during OER in H₂¹⁶O/0.1 M HClO₄. With gradual increase in OER current (Fig. 4d, top and Supplementary Fig. 40a), a corresponding increase in both ³²O₂ (¹⁶O + ¹⁶O) and ³⁴O₂ (¹⁶O + ¹⁸O) signal was detected (Fig. 4d, middle and Supplementary Fig. 40b). The signal ratio of ³⁴O₂:³²O₂ within the OER potential range (Fig. 4d, bottom and Supplementary Fig. 40c) remained relatively constant and is comparable to that of the natural abundance of ¹⁸O in deionized water within experimental uncertainty^{33,49}, suggesting that the LOM mechanism did not occur over both RuO₂ and Ni-RuO₂. The DEMS analysis, coupled with galvanostatic measurement, further confirmed this conclusion (Supplementary Figs. 41 and 42), in which the constant ³²O₂ and ³⁴O₂ signals and ³⁴O₂:³²O₂ ratio were clearly observed. Our DEMS results are consistent with previous reports that also suggest the exclusivity of AEM over RuO₂-based OER catalysts⁴⁷⁻⁴⁹.

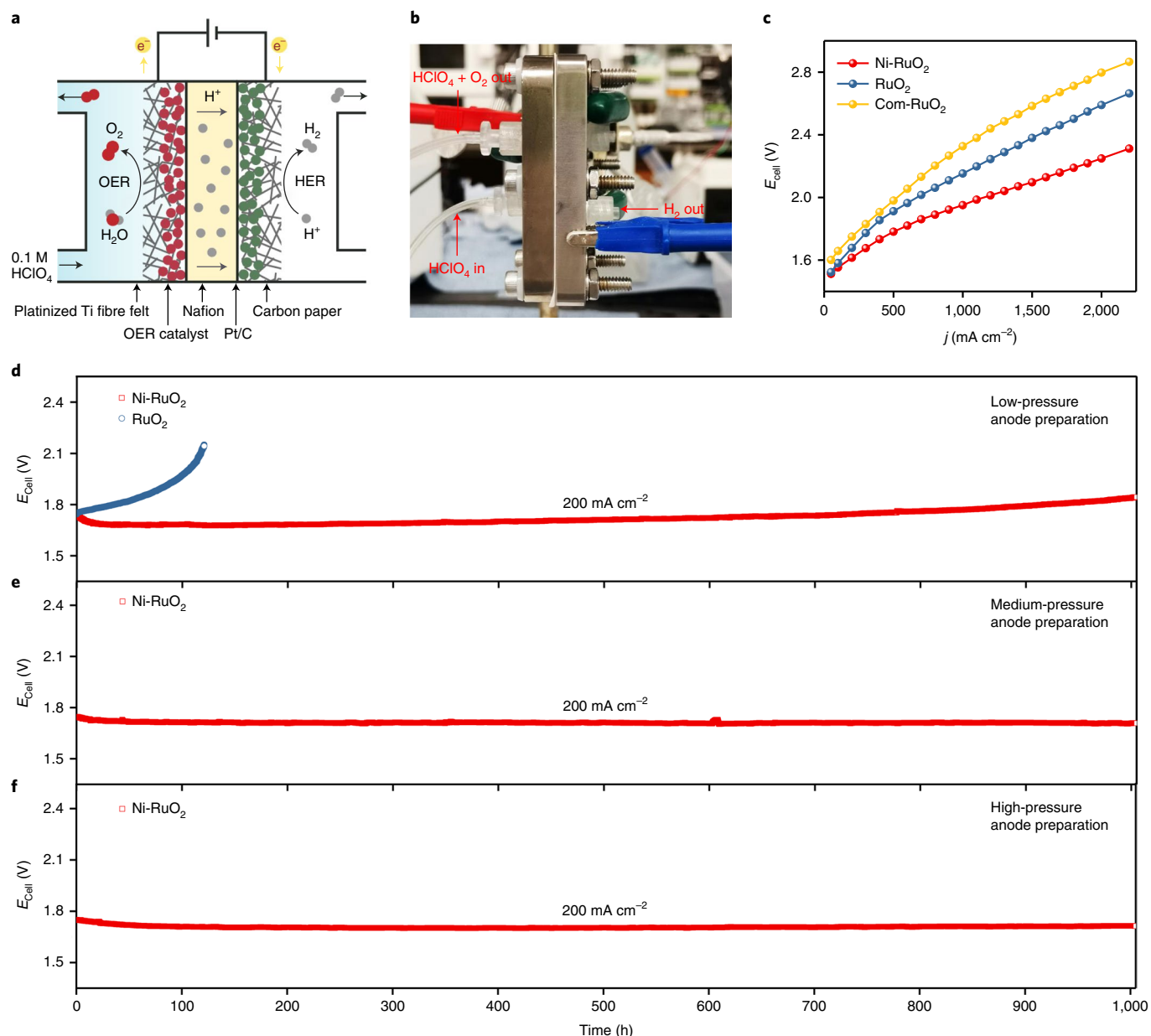


Fig. 5 | PEM-WE device performance using Ni-RuO₂ as an acidic OER catalyst at room temperature and ambient pressure. a, b, Schematic (a) and photograph (b) of the PEM-WE device. **c**, I-V curves of PEM-WE electrolyzers using Ni-RuO₂, RuO₂ or Com-RuO₂ as anodic catalyst and commercial Pt/C as cathodic catalyst, at room temperature and ambient pressure. No cell voltages

were iR compensated. **d-f**, Chronopotentiometry testing of Ni-RuO₂ and RuO₂ catalysts at 200 mA cm⁻² in the PEM-WE electrolyser using commercial Pt/C as the cathode catalyst, at room temperature and ambient pressure. The Ni-RuO₂ catalyst coating in these stability tests was press-prepared under low pressure (<0.5 MPa) (d), medium pressure (-1.5 MPa) (e) and high pressure (-3.0 MPa) (f).

With the OER pathway determined on the RuO₂ surface, the impacts of the incorporation of Ni on activity and stability could be evaluated via limiting potential and lattice stability calculations, respectively. First, the limiting potential of OER on the Ni-RuO₂ (110) surface was predicted to be 1.70 V (Fig. 4e), which is about 0.2 V lower than that of RuO₂ and suggests improved OER activity. Regarding stability, we first evaluated enthalpy change for the surface Ru atom demetallation process from the surface of both RuO₂ and Ni-RuO₂ (110), because delamination of surface Ru atoms may contribute to the low stability of catalysts³⁶. The proposed demetallation process of Ru is presented in Supplementary Figs. 43 and 44, in which Ru at the CUS Ru site moves away from the (110) surface. We found that with incorporation of Ni into the lattice, the energy cost for Ru demetallation increased from 1.87

to 2.22 eV (Fig. 4f, left), suggesting a more stable surface Ru in Ni-RuO₂ than in RuO₂. Computational results of the demetallation process are further discussed in Supplementary Note 2 and Supplementary Table 3. To evaluate lattice oxygen stability, we calculated the enthalpy change of the subsurface oxygen loss process (Supplementary Fig. 45)^{24,50}. The enthalpy changes for subsurface oxygen loss were calculated to be 1.67 and 2.12 eV (Fig. 4f, right) on the RuO₂ and Ni-RuO₂ (110) surface, respectively, clearly suggesting that the introduction of Ni dopants to the RuO₂ lattice had also stabilized lattice oxygen during OER. Consequently, our DFT simulations show that incorporation of Ni improves the OER stability of RuO₂ by hindering both surface Ru demetallation and lattice oxygen loss, supporting our experimental observations of significantly improved OER stability in the Ni-RuO₂ catalyst.

PEM–WE device performance

Finally, to investigate the practical application potential of our Ni–RuO₂ catalyst for water electrolysis, we constructed a PEM–WE electrolyser using Ni–RuO₂ as the anode catalyst for OER, commercial Pt/C as the cathode catalyst for HER and a proton exchange membrane (Nafion 117; Fig. 5a,b). Pt/C was chosen due to its well-known properties of high durability and activity in HER. The current–voltage characteristic (I–V) curves (without iR compensation) in Fig. 5c clearly show that the Ni–RuO₂/PEM/Pt/C electrolyser had improved water electrolysis activity compared with the RuO₂ and Com–RuO₂ electrolysers. Specifically, the Ni–RuO₂-based electrolyser (at room temperature) required only 1.78, 1.95 and 2.10 V to reach a current density of 500, 1,000 and 1,500 mA cm⁻², respectively (Fig. 5c). Of note, due to the lack of specific expertise and equipment in the fabrication of an industrial-level quality membrane electrode with minimal ionic resistance between cathode and anode, our device still presents impedance of ~0.3 Ω cm⁻², contributing ~300 mV of iR drop at 1 A cm⁻². This, however, does not affect the evaluation of our catalyst's intrinsic activity (as shown in our standard three-electrode set-up) or the following durability tests.

Catalyst stability could play an even more important role than its activity in practical applications; we thus evaluated the stability of our Ni–RuO₂-based electrolyser, as well as pristine RuO₂ for comparison, at 200 mA cm⁻² (Fig. 5d). The voltage of the RuO₂ electrolyser was clearly increased following ~120 h of electrolysis, suggesting poor OER stability under practical operation conditions (Fig. 5d). Remarkably, our Ni–RuO₂ catalyst showed markedly improved PEM–WE durability: it was operated for 1,000 h with only a small cell voltage increase in our initial trial (Fig. 5d). We suspected the slight degradation in cell performance observed from ~700 h was probably due to detachment of the Ni–RuO₂ catalyst from the anode electrode during prolonged anolyte circulation and gas bubble evolution, because we observed the presence of some black material (most probably the catalyst) coated on the inner surface of the anolyte outlet tube after the stability test (Supplementary Fig. 46). We thus used an improved and stronger coating method to further explore the durability of the Ni–RuO₂ catalyst (Methods). The stability of two newly prepared anodes was further improved (Fig. 5e,f): no obvious cell voltage increase was observed for these during 1,000 h stability tests. Additionally, much less black material was observed on the inner surface of the anolyte outlet tubes after stability tests compared with the initial trial (Supplementary Fig. 47). RuO₂ still showed much lower stability than Ni–RuO₂ after electrode preparation optimization (Supplementary Fig. 48). The faradaic efficiencies of O₂ generated by the PEM–WE cell were measured as ~100% for Ni–RuO₂ (Supplementary Fig. 49a). We monitored Ru dissolution from the Ni–RuO₂ catalyst by ICP–MS during the 1,000 h stability test (Supplementary Fig. 49b). A rapid increase in Ru concentration was observed at the very beginning of the operation, which could be ascribed to the dissolution of unstable Ru species during the catalyst activation process. Ru dissolution was gradually stabilized within the first 500 h and remain nearly unchanged, at ~30 ppb, for the remainder of the stability test. Additionally, our Ni–RuO₂ catalyst can also be stably operated under an elevated electrolyte temperature for >1,000 h without obvious performance degradation (Supplementary Fig. 50). These stability results clearly demonstrate the great potential of our Ni–RuO₂ catalyst for future practical applications.

In summary, we developed a non-iridium-based acidic OER catalyst that can deliver at least 1,000 h of stability under a 200-mA cm⁻² water-splitting current in a PEM–WE device. The findings in this work not only provide an effective method and new understanding to improving catalytic performance of the RuO₂ catalyst, but also demonstrate its great future potential for implementation in practical PEM cells for large-scale clean H₂ generation. While there is still a gap between our Ni–RuO₂ catalyst's stability performance and the typical industrial requirement (delivering >1 A cm⁻² current for over 10 years of operation at 80 °C), this encouraging milestone stability that we

achieved using a Ru-based catalyst clearly suggests the potential of replacing Ir-based catalysts in the future. More studies can be carried out in the future to further improve the stability of Ru-based catalysts, such as temperature effects, multi-element doping and so on.

Online content

Any methods, additional references, Nature Research reporting summaries, source data, extended data, supplementary information, acknowledgements, peer review information; details of author contributions and competing interests; and statements of data and code availability are available at <https://doi.org/10.1038/s41563-022-01380-5>.

References

1. Turner, J. A. Sustainable hydrogen production. *Science* **305**, 972–974 (2004).
2. Chu, S. & Majumdar, A. Opportunities and challenges for a sustainable energy future. *Nature* **488**, 294–303 (2012).
3. Seh, Z. W. et al. Combining theory and experiment in electrocatalysis: insights into materials design. *Science* **355**, eaad4998 (2017).
4. Carmo, M., Fritz, D. L., Mergel, J. & Stolten, D. A comprehensive review on PEM water electrolysis. *Int. J. Hydrog. Energy* **38**, 4901–4934 (2013).
5. An, L. et al. Recent development of oxygen evolution electrocatalysts in acidic environment. *Adv. Mater.* **33**, 2006328 (2021).
6. Spöri, C., Kwan, J. T. H., Bonakdarpour, A., Wilkinson, D. P. & Strasser, P. The stability challenges of oxygen evolving catalysts: towards a common fundamental understanding and mitigation of catalyst degradation. *Angew. Chem. Int. Ed. Engl.* **56**, 5994–6021 (2017).
7. King, L. A. et al. A non-precious metal hydrogen catalyst in a commercial polymer electrolyte membrane electrolyser. *Nat. Nanotechnol.* **14**, 1071–1074 (2019).
8. Li, L., Wang, P., Shao, Q. & Huang, X. Recent progress in advanced electrocatalyst design for acidic oxygen evolution reaction. *Adv. Mater.* **33**, e2004243 (2021).
9. Chen, F.-Y., Wu, Z.-Y., Adler, Z. & Wang, H. Stability challenges of electrocatalytic oxygen evolution reaction: from mechanistic understanding to reactor design. *Joule* **5**, 1704–1731 (2021).
10. Seitz, L. C. et al. A highly active and stable IrO₂/SrIrO₃ catalyst for the oxygen evolution reaction. *Science* **353**, 1011–1014 (2016).
11. Chatti, M. et al. Intrinsically stable in situ generated electrocatalyst for long-term oxidation of acidic water at up to 80 °C. *Nat. Catal.* **2**, 457–465 (2019).
12. Yao, Y. et al. Engineering the electronic structure of single atom Ru sites via compressive strain boosts acidic water oxidation electrocatalysis. *Nat. Catal.* **2**, 304–313 (2019).
13. Wen, Y. et al. Stabilizing highly active Ru sites by suppressing lattice oxygen participation in acidic water oxidation. *J. Am. Chem. Soc.* **143**, 6482–6490 (2021).
14. Reier, T. et al. Molecular insight in structure and activity of highly efficient, low-Ir Ir–Ni oxide catalysts for electrochemical water splitting (OER). *J. Am. Chem. Soc.* **137**, 13031–13040 (2015).
15. Song, J. et al. A review on fundamentals for designing oxygen evolution electrocatalysts. *Chem. Soc. Rev.* **49**, 2196–2214 (2020).
16. Moreno-Hernandez, I. A. et al. Crystalline nickel manganese antimonate as a stable water-oxidation catalyst in aqueous 1.0 M H₂SO₄. *Energy Environ. Sci.* **10**, 2103–2108 (2017).
17. Geiger, S. et al. The stability number as a metric for electrocatalyst stability benchmarking. *Nat. Catal.* **1**, 508–515 (2018).
18. Diaz-Morales, O. et al. Iridium-based double perovskites for efficient water oxidation in acid media. *Nat. Commun.* **7**, 12363 (2016).

19. Hao, S. et al. Torsion strained iridium oxide for efficient acidic water oxidation in proton exchange membrane electrolyzers. *Nat. Nanotechnol.* **16**, 1371–1377 (2021).
20. Zheng, Y.-R. et al. Monitoring oxygen production on mass-selected iridium–tantalum oxide electrocatalysts. *Nat. Energy* **7**, 55–64 (2022).
21. Su, J. et al. Assembling ultrasmall copper-doped ruthenium oxide nanocrystals into hollow porous polyhedra: highly robust electrocatalysts for oxygen evolution in acidic media. *Adv. Mater.* **30**, 1801351 (2018).
22. Retuerto, M. et al. Na-doped ruthenium perovskite electrocatalysts with improved oxygen evolution activity and durability in acidic media. *Nat. Commun.* **10**, 2041 (2019).
23. Lin, Y. et al. Chromium-ruthenium oxide solid solution electrocatalyst for highly efficient oxygen evolution reaction in acidic media. *Nat. Commun.* **10**, 162 (2019).
24. Hao, S. et al. Dopants fixation of Ruthenium for boosting acidic oxygen evolution stability and activity. *Nat. Commun.* **11**, 5368 (2020).
25. Jin, H. et al. Safeguarding the RuO₂ phase against lattice oxygen oxidation during acidic water electrooxidation. *Energy Environ. Sci.* **15**, 1119–1130 (2022).
26. Cao, L. et al. Dynamic oxygen adsorption on single-atomic Ruthenium catalyst with high performance for acidic oxygen evolution reaction. *Nat. Commun.* **10**, 4849 (2019).
27. Chen, S. et al. Mn-doped RuO₂ nanocrystals as highly active electrocatalysts for enhanced oxygen evolution in acidic media. *ACS Catal.* **10**, 1152–1160 (2020).
28. Halck, N. B., Petrykin, V., Krtil, P. & Rossmeisl, J. Beyond the volcano limitations in electrocatalysis – oxygen evolution reaction. *Phys. Chem. Chem. Phys.* **16**, 13682–13688 (2014).
29. Wang, J. et al. Transition metal-doped ultrathin RuO₂ networked nanowires for efficient overall water splitting across a broad pH range. *J. Mater. Chem. A Mater.* **7**, 6411–6416 (2019).
30. Zhao, Z. L. et al. Boosting the oxygen evolution reaction using defect-rich ultra-thin ruthenium oxide nanosheets in acidic media. *Energy Environ. Sci.* **13**, 5143–5151 (2020).
31. Hubert, M. A. et al. Acidic oxygen evolution reaction activity–stability relationships in Ru-based pyrochlores. *ACS Catal.* **10**, 12182–12196 (2020).
32. Cui, X. et al. Robust interface Ru centers for high-performance acidic oxygen evolution. *Adv. Mater.* **32**, 1908126 (2020).
33. Grimaud, A. et al. Activating lattice oxygen redox reactions in metal oxides to catalyse oxygen evolution. *Nat. Chem.* **9**, 457–465 (2017).
34. Wohlfahrt-Mehrens, M. & Heitbaum, J. Oxygen evolution on Ru and RuO₂ electrodes studied using isotope labelling and on-line mass spectrometry. *J. Electroanal. Chem. Interfacial Electrochem.* **237**, 251–260 (1987).
35. Klyukin, K., Zagalskaya, A. & Alexandrov, V. Role of dissolution intermediates in promoting oxygen evolution reaction at RuO₂(110) surface. *J. Phys. Chem. C Nanomater. Interfaces* **123**, 22151–22157 (2019).
36. Zagalskaya, A. & Alexandrov, V. Role of defects in the interplay between adsorbate evolving and lattice oxygen mechanisms of the oxygen evolution reaction in RuO₂ and IrO₂. *ACS Catal.* **10**, 3650–3657 (2020).
37. Cherevko, S. Stability and dissolution of electrocatalysts: building the bridge between model and ‘real world’ systems. *Curr. Opin. Electrochem.* **8**, 118–125 (2018).
38. Xu, S.-L. et al. High-temperature synthesis of small-sized Pt/Nb alloy catalysts on carbon supports for hydrothermal reactions. *Inorg. Chem.* **59**, 15953–15961 (2020).
39. Yu, M. et al. Scalable self-growth of Ni@NiO core-shell electrode with ultrahigh capacitance and super-long cyclic stability for supercapacitors. *NPG Asia Mater.* **6**, e129–e129 (2014).
40. Wu, Z.-Y. et al. Partially oxidized Ni nanoparticles supported on Ni-N co-doped carbon nanofibers as bifunctional electrocatalysts for overall water splitting. *Nano Energy* **51**, 286–293 (2018).
41. Feng, Q. et al. Highly active and stable ruthenate pyrochlore for enhanced oxygen evolution reaction in acidic medium electrolysis. *Appl. Catal. B* **244**, 494–501 (2019).
42. Over, H. Surface chemistry of ruthenium dioxide in heterogeneous catalysis and electrocatalysis: from fundamental to applied research. *Chem. Rev.* **112**, 3356–3426 (2012).
43. Rochefort, D., Dabo, P., Guay, D. & Sherwood, P. M. A. XPS investigations of thermally prepared RuO₂ electrodes in reductive conditions. *Electrochim. Acta* **48**, 4245–4252 (2003).
44. Chen, Y. et al. Exceptionally active iridium evolved from a pseudo-cubic perovskite for oxygen evolution in acid. *Nat. Commun.* **10**, 572 (2019).
45. Kim, Y. D., Schwegmann, S., Seitsonen, A. P. & Over, H. Epitaxial growth of RuO₂(100) on Ru(1010): surface structure and other properties. *J. Phys. Chem. B* **105**, 2205–2211 (2001).
46. Heras-Domingo, J., Sodupe, M. & Solans-Monfort, X. Interaction between ruthenium oxide surfaces and water molecules. Effect of surface morphology and water coverage. *J. Phys. Chem. C Nanomater. Interfaces* **123**, 7786–7798 (2018).
47. Rao, R. R. et al. Towards identifying the active sites on RuO₂(110) in catalyzing oxygen evolution. *Energy Environ. Sci.* **10**, 2626–2637 (2017).
48. Rao, R. R. et al. Operando identification of site-dependent water oxidation activity on ruthenium dioxide single-crystal surfaces. *Nat. Catal.* **3**, 516–525 (2020).
49. Stoerzinger, K. A. et al. Orientation-dependent oxygen evolution on RuO₂ without lattice exchange. *ACS Energy Lett.* **2**, 876–881 (2017).
50. Rong, X., Parolin, J. & Kolpak, A. M. A fundamental relationship between reaction mechanism and stability in metal oxide catalysts for oxygen evolution. *ACS Catal.* **6**, 1153–1158 (2016).

Publisher’s note Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional affiliations.

Springer Nature or its licensor holds exclusive rights to this article under a publishing agreement with the author(s) or other rightsholder(s); author self-archiving of the accepted manuscript version of this article is solely governed by the terms of such publishing agreement and applicable law.

© The Author(s), under exclusive licence to Springer Nature Limited 2022

Methods

Synthesis of catalysts

In a typical procedure, 0.1721 g of RuCl_3 and 0.0656 g of $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$ (that is, RuCl_3 and NiCl_2 at a molar ratio of 3:1) were mixed in 150 ml of 1 M HCl and sonicated for 2 h. Carbon black (0.4 g; Cabot, BP2000) was then added and dispersed by stirring for 18 h under room temperature to ensure uniform distribution. Next, the mixture was dried by using a rotary evaporator and the remaining powder was collected. The powder was annealed in a flowing Ar/H_2 (5% H_2) atmosphere at 900 °C for 2 h and then annealed in air at 250–550 °C (450 °C as the optimized temperature) for 3 h. After annealing, 50 mg of product was added to 20 ml of 1 M HCl and mixed at room temperature for 12 h to perform acid leaching, then centrifuged and washed with deionized water three times. Finally, the sample was dried at 80 °C in an oven for 12 h to obtain the Ni-RuO₂ catalyst. $\text{Ru}_a\text{Ni}_b\text{O}_x$ -AL samples with different amounts of Ni dopant were also prepared following the same procedure, except that the level of precursors was tuned in the first step. In addition, RuO_2 with no Ni incorporated was prepared in a similar method using RuCl_3 as precursor. M-RuO₂ (M=Fe, Co, Zn, Cu) samples with different metal dopants were also prepared using the same procedure, except that the precursors used in the first step were different— FeCl_3 , CoCl_2 , $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, and $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$. Of note, the weight ratio of total metal content in precursors to carbon black support was fixed at 1:4 in all catalyst synthesis.

Characterization

TEM, HAADF-STEM and EDS elemental mapping were performed on a Talos F200X transmission electron microscope (at an accelerating voltage of 200 kV) equipped with an energy-dispersive detector. HR-TEM and HR-HAADF-STEM images were captured using a JEM-ARM 200 F atomic resolution analytical microscope operating at an accelerating voltage of 200 kV. XPS data were obtained on an X-ray photoelectron spectrometer (ESCALab MKII) with an excitation source of Mg K α radiation (1,253.6 eV). XRD data were collected on a Rigaku SmartLab X-ray diffractometer. XAS measurements were conducted at the Sector 20-BM beamline of the Advanced Photon Source at Argonne National Laboratory. All XAS measurements were carried out at room temperature under ambient pressure. Samples were measured simultaneously in fluorescence mode with metal foils as reference. Data processing and EXAFS fitting were performed using the Athena program. The XAS data of NiO and Ni references are from our previous work⁵¹.

Electrochemical measurements under a three-electrode system

In a typical test, 5 mg of catalyst was added to 1 ml of isopropyl alcohol and 20 μl of Nafion-117-containing solution (5%; Sigma-Aldrich) and sonicated for 1 h to obtain a well-dispersed catalyst ink. For electrode preparation, 16 μl of catalyst ink was drop-cast on a 5.0-mm-diameter glassy carbon electrode (disk geometric area, 0.196 cm²), resulting in a catalyst loading of 0.4 mg cm⁻², and then vacuum dried at room temperature before usage. All RDE measurements were run at room temperature in a typical three-electrode cell in an O₂-saturated 0.1 M HClO₄ electrolyte. A carbon rod (99.99%; Beantown Chemical) and a saturated calomel electrode (SCE, CH Instruments) were used as the counter and reference electrode, respectively. An RDE assembly (no. AFE4TQ050, Pine Instruments) with the prepared glassy carbon electrode were used as the working electrode, at a rotation rate of 2,500 r.p.m. In this work, all potentials measured against SCE were converted to the reversible hydrogen electrode (RHE) scale using: E (potential, versus RHE) = E (versus SCE) + 0.241 V + 0.0591 \times pH. In 0.1 M HClO₄ electrolyte, pH values are all equal to 1.0 in this work as determined by an Orion Star A111 pH meter (Thermo Scientific). Solution resistance (R_s) was measured by potentiostatic electrochemical impedance spectroscopy at frequencies ranging from 0.1 Hz to 200 kHz. All measured potentials in RDE tests were 100% iR compensated unless otherwise specified. LSV tests were recorded at a scan rate of 5 mV s⁻¹.

Stability was examined by chronopotentiometry testing at 10 mA cm⁻². EIS tests were performed at 1.45 V (versus RHE) from 0.1 Hz to 200 kHz, and the results are presented in the form of a Nyquist plot. The ECSA was determined by: $\text{ECSA} = C_{\text{dl}}/C_s$, where C_{dl} is double-layer capacitance and C_s the specific capacitance of the sample. In this study, a general specific capacitance of $C_s = 0.035 \text{ mF cm}^{-2}$ was used based on typical reported values²³. C_{dl} was determined by the equation $C_{\text{dl}} = i_c/v$, where i_c is the charging current and v the scan rate. A series of CV tests in the non-faradaic potential region 1.18–1.28 V (versus RHE) under different scan rates (2.5, 5.0, 7.5, 10, 15 and 20 mV s⁻¹) were performed. And by plotting measured i_c versus v , C_{dl} was obtained from the slopes of the linear fitting. The roughness factor was calculated by dividing ECSA by the geometric area of the electrode, which was 0.196 cm² in this study. The S-number¹⁷ was calculated using the following equation:

$$S = \frac{n_{\text{O}_2}}{n_{\text{Ru(dissolved)}}}$$

where n_{O_2} is the molar number of total oxygen evolved within a certain period of time (calculated from total charge) and $n_{\text{Ru(dissolved)}}$ is total dissolved Ru as measured by ICP-MS.

DEMS tests

One milligram of catalyst was mixed with 10 wt% of Nafion in 0.5 ml of ethanol and then drop-cast onto the glassy carbon (0.5-mm diameter) working electrode. The electrode was dried at room temperature for at least 1 h before testing. Measurement was performed on a HPR-40 DEMS (Hiden Analytical) coupled to the flow cell illustrated in Fig. 4d, an Autolab potentiostat (no. PGSTAT204, Metrohm), an OER catalyst modified working electrode, an Ag/AgCl reference electrode and a Pt wire counter electrode. Electrolyte flow rate was controlled at 0.5 ml min⁻¹. All electrochemical results were recorded versus the reference electrode and converted to RHE following the relationship $E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.197 + 0.0591 \times \text{pH}$. Catalysts were first labelled with ¹⁸O in 0.1 M HClO₄ solution created with ¹⁸O-labelled water (97% ¹⁸O; Cambridge Isotope Laboratories) for 10 min at 10 mA cm⁻². Electrodes and cell were then rinsed with ¹⁶O water for 20 min to remove any H₂¹⁸O residual and scanned in a 0.1 M HClO₄ solution of H₂¹⁶O at 0.5 mV s⁻¹ from 1.1 V versus RHE until current density reached 50 mA cm⁻². An electron energy of 70 eV was used for ionization of all species, with an emission current of 450 μA . All mass-selected product ($m/z = 32$ and 34) was detected by a secondary electron multiplier with a detector voltage of 1,200 V. Data were averaged every ten points to yield a smoother MS signal, and m/z 34/32 signals were calculated with the fitting data. For DEMS measurements using the galvanostatic method, after labelling and rinsing (as mentioned above) the background was collected for 10 min before the application of 10 mA cm⁻² for 30 min to probe potential oxygen lattice exchange.

PEM-WE tests

For electrolyser tests, a self-made cell was used as the PEM-WE device and a cation exchange membrane (Nafion 117) as the membrane electrolyte. Around 0.65 mg cm⁻² commercial Pt/C with 20 wt.% Nafion 117 binder was air-brushed onto a carbon paper electrode as an HER cathode. In our initial trial (Fig. 5d), -3.1 mg cm⁻² OER catalyst with 20 wt.% polytetrafluoroethylene binder was drop-cast onto a platinized titanium fibre felt electrode. After drying, the electrode was pressed at room temperature under a low pressure of <0.5 MPa by a regular hot-press machine. The electrode was then annealed in air for 30 min at 350 °C and used as an OER anode, which was then circulated with 0.1 M HClO₄ aqueous solution at 4 ml min⁻¹. I-V curves were measured in galvanostatic mode at 50–2,200 mA cm⁻² at room temperature and ambient pressure. The stability test was carried out at 200 mA cm⁻² at room temperature and ambient pressure. To further improve the stability of the Ni-RuO₂-based PEM-WE device (Fig. 5e,f), we optimized the electrode preparation process. The Ni-RuO₂ catalyst was freshly annealed at 450 °C before use. We performed the same drop-casting process of Ni-RuO₂ onto a platinized titanium fibre felt electrode. The Ni-RuO₂-coated electrode was then pressed under medium (-1.5 MPa) or high pressure

(-3.0 MPa) by a hydraulic press machine at room temperature, followed by the same annealing process (350 °C for 30 min) to prepare the final OER anode. We then performed stability tests at 200 mA cm⁻² at room temperature and ambient pressure. Additionally, to reduce electrolyte flushing on the anode coating, we reduced the anolyte circulation flow rate from 4 ml min⁻¹ in our initial trial to 0.5 ml min⁻¹ for medium- and high-pressure-prepared anode-based electrolysers, at room temperature and ambient pressure. All cell voltages measured in PEM-WE electrolysers were reported without iR compensation. Please be aware here that the slight voltage difference between I-V curves and chronopotentiometry stability tests may have arisen from the different electrolysers activation processes or electrolyser resistances.

Computational details

First-principles DFT^{52,53} calculations with a plane-wave basis set were performed using Vienna ab initio simulation package^{54,55} software. The Perdew, Burke and Ernzerhof functionals of generalized gradient approximation⁵⁶ were used to describe the terms of electronic exchange and correlation energy. The energy cut-off of the plane-wave basis was set at 500 eV for plane-wave expansion. Projector-augmented wave^{57,58} pseudo-potential was used to describe the core electrons. Electronic energy was converged until the energy difference between iterations was <10⁻⁵ eV. During structure optimization calculations, atomic positions were relaxed until the force on each ion was <0.01 eV Å⁻¹. The lattice parameters of rutile RuO₂ were determined as: a = 4.53 Å and c = 3.12 Å, in agreement with a previous computational prediction³⁶ of a = 4.54 Å and c = 3.14 Å. A 2 × 2 × 1 RuO₂ (110) model with 16 Ru atoms and 32 O atoms was used in our calculations. The slab model consisted of two atomic layers each of O and Ru; the top two layers (one each of O and Ru) were optimized during structure optimization calculations. A vacuum layer of 15 Å thickness was added perpendicularly to the surface to minimize the interaction between periodic images. To model the Ni-doped RuO₂ surface, one Ru atom at a bridge site in the 2 × 2 × 1 RuO₂ (110) model was substituted by a Ni atom, leading to a chemical composition of 2.1 at percentage Ni, 31.3 at percentage Ru and 66.6 at percentage O. The Brillouin zone was sampled using the Monkhorst⁵⁹ scheme with 6 × 3 × 1 k-point mesh for RuO₂ (110) and Ni-RuO₂ (110). Due to the strong correlation of *d* electrons in Ni, a *U*-*J* value of 5.3 eV was adopted⁶⁰. Zero-point energy corrections, ZPE, were included in all adsorbate system calculations. These were calculated as $ZPE = \sum_i \frac{1}{2} h \nu_i$, where *h* is Planck's constant and *ν*_{*i*} is the frequency of the *i*th vibrational mode of binding molecules.

Data availability

The data that support the findings of this study are presented in the main text and the Supplementary Information, and are available from the corresponding authors upon reasonable request.

References

- Wu, Z.-Y. et al. Electrochemical ammonia synthesis via nitrate reduction on Fe single atom catalyst. *Nat. Commun.* **12**, 2870 (2021).
- Hohenberg, P. & Kohn, W. Inhomogeneous electron gas. *Phys. Rev.* **136**, B864–B871 (1964).
- Kohn, W. & Sham, L. J. Self-consistent equations including exchange and correlation effects. *Phys. Rev.* **140**, A1133–A1138 (1965).
- Kresse, G. & Furthmüller, J. Efficiency of ab-initio total energy calculations for metals and semiconductors using a plane-wave basis set. *Comp. Mater. Sci.* **6**, 15–50 (1996).
- Kresse, G. & Hafner, J. Ab initio molecular dynamics for liquid metals. *Phys. Rev. B* **47**, 558–561 (1993).
- Perdew, J. P., Burke, K. & Ernzerhof, M. Generalized gradient approximation made simple. *Phys. Rev. Lett.* **77**, 3865–3868 (1996).
- Blöchl, P. E. Projector augmented-wave method. *Phys. Rev. B* **50**, 17953–17979 (1994).
- Kresse, G. & Joubert, D. From ultrasoft pseudopotentials to the projector augmented-wave method. *Phys. Rev. B* **59**, 1758–1775 (1999).
- Monkhorst, H. J. & Pack, J. D. Special points for Brillouin-zone integrations. *Phys. Rev. B* **13**, 5188–5192 (1976).
- Dudarev, S. L., Botton, G. A., Savrasov, S. Y., Humphreys, C. J. & Sutton, A. P. Electron-energy-loss spectra and the structural stability of nickel oxide: an LSDA+U study. *Phys. Rev. B* **57**, 1505–1509 (1998).

Acknowledgements

This work was supported by the Welch Foundation Research (grant no. C-2051-20200401), the David and Lucile Packard Foundation Packard Fellowship programme (grant no. 2020–71371) and the Roy E. Campbell Faculty Development Award. B.L. and G.W. gratefully acknowledge financial support for this research provided by the National Science Foundation (NSF) (grant no. DMR 1905572). S.Z. and S.-W.Y. gratefully acknowledge the financial support for this research provided by the NSF (grant no. CBET- 2004808). This work also used the computational resources provided by the University of Pittsburgh Center for Research Computing, and the resources of the Advanced Photon Source, a US Department of Energy (DOE) Office of Science User Facility operated for the DOE Office of Science by the Argonne National Laboratory under contract no. DE-AC02-06CH11357.

Author contributions

Z.-Y.W. and H.W. conceived the project. H.W., G.W. and S.Z. supervised the project. Z.-Y.W. developed the synthesis of catalysts. Z.-Y.W. and F.-Y.C. performed catalyst synthesis, catalytic tests and related data processing. Z.-Y.W., F.-Y.C., Y.Z.F., D.M.M. and P.Z. performed materials characterization. Q.-Q.Y., M.-X.C., T.-W.S. and H.-W.L. kindly helped with TEM and XAS data analysis. S.-W.Y., Z.Y. and S.Z. performed DEMS testing. B.L. and G.W. performed DFT simulation. Z.-Y.W., F.-Y.C., B.L., H.W. and G.W. co-wrote the manuscript. All authors discussed the results and commented on the manuscript.

Competing interests

A patent application has been filed based on this study.

Additional information

Supplementary information The online version contains supplementary material available at <https://doi.org/10.1038/s41563-022-01380-5>.

Correspondence and requests for materials should be addressed to Sen Zhang, Guofeng Wang or Haotian Wang.

Peer review information *Nature Materials* thanks the anonymous reviewers for their contribution to the peer review of this work.

Reprints and permissions information is available at www.nature.com/reprints.